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APPLICATION NUMBER: 10/083,778

FILING DATE: February 25, 2002

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UTILITY PATENT APPLICATION TRANSMITTAL

(Only for new nonprovisional applications under 37 CFR 1.53(b))

APPLICATION ELEMENTS

See MPEP chapter 600 concerning utility patent application contents.

1. Fee Transmittal Form (e.g., PTO/SB/17)
(Submit an original and a duplicate for fee processing)
2. Applicant claims small entity status.
See 37 CFR 1.27.
3. Specification [Total Pages 25] *(preferred arrangement set forth below)*
 - Descriptive title of the invention
 - Cross Reference to Related Applications
 - Statement Regarding Fed sponsored R & D
 - Reference to sequence listing, a table, or a computer program listing appendix
 - Background of the Invention
 - Brief Summary of the Invention
 - Brief Description of the Drawings *(if filed)*
 - Detailed Description
 - Claim(s)
 - Abstract of the Disclosure
4. Drawing(s) (35 U.S.C. 113) [Total Sheets 2]
5. Oath or Declaration [Total Pages 3]
 - a. Newly executed (original or copy)
Copy from a prior application (37 CFR 1.63 (d))
(for continuation/divisional with Box 17 completed)
 - b. **DELETION OF INVENTOR(S)**
Signed statement attached deleting Inventor(s)
named in the prior application, see 37 CFR
1.63(d)(2) and 1.33(b).
6. Application Data Sheet. See 37 CFR 1.76

17. If a CONTINUING APPLICATION, check appropriate box, and supply the requisite information below and in a preliminary amendment, or in an Application Data Sheet under 37 CFR 1.76:

Continuation Divisional Continuation-in-part (CIP)

of prior application No.: _____

Prior application Information:

Examiner _____

Group / Art Unit: _____

For CONTINUATION OR DIVISIONAL APPS only: The entire disclosure of the prior application, from which an oath or declaration is supplied under Box 5b, is considered a part of the disclosure of the accompanying continuation or divisional application and is hereby incorporated by reference. The incorporation can only be relied upon when a portion has been omitted.

**23543**

Air Products and Chemicals, Inc.

 Customer Number or Bar Code Label Correspondence address below

Name _____

Address _____

Address _____

State _____

Zip Code _____

Country _____

Telephone _____

Fax _____

Name (Print/Type)	Robert J. Wolff	Registration No. (Attorney/Agent)	34,948
Signature		Date	Feb. 25, 2002

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FEE TRANSMITTAL for FY 2002

Patent fees are subject to annual revision.

TOTAL AMOUNT OF PAYMENT (\$ 1,226.00)

Complete if Known

Application Number	
Filing Date	
First Named Inventor	Shou-I Wang
Examiner Name	
Group Art Unit	
Attorney Docket No.	06244 USA

METHOD OF PAYMENT

1. The Commissioner is hereby authorized to charge indicated fees and credit any overpayments to:

Deposit Account Number **01-0493**

Deposit Account Name **Air Products and Chemicals, Inc.**

Charge Any Additional Fee Required Under 37 CFR 1.16 and 1.17

Applicant claims small entity status. See 37 CFR 1.27

2. Payment Enclosed:
 Check Credit card Money Order Other

FEE CALCULATION

1. BASIC FILING FEE

Large Entity Fee Code (\$)	Small Entity Fee Code (\$)	Fee Description	Fee Paid
101 740	201 370	Utility filing fee	740.00
106 330	206 165	Design filing fee	
107 510	207 255	Plant filing fee	
108 740	208 370	Reissue filing fee	
114 160	214 80	Provisional filing fee	

SUBTOTAL (1) (\$ 740)

2. EXTRA CLAIM FEES

Total Claims	Extra Claims	Fee from below	Fee Paid
33	-20* = 13	x 18	= 234
6	-3** = 3	x 84	= 252

Large Entity Fee Code (\$)	Small Entity Fee Code (\$)	Fee Description
103 18	203 9	Claims in excess of 20
102 84	202 42	Independent claims in excess of 3
104 280	204 140	Multiple dependent claim, if not paid
109 84	209 42	** Reissue Independent claims over original patent
110 18	210 9	** Reissue claims in excess of 20 and over original patent

SUBTOTAL (2) (\$ 486)

*or number previously paid, if greater; For Reissues, see above

FEE CALCULATION (continued)

3. ADDITIONAL FEES

Fee Code	Large Entity Fee (\$)	Small Entity Fee (\$)	Fee Description	Fee Paid
105	130	205	85 Surcharge - late filing fee or oath	
127	50	227	25 Surcharge - late provisional filing fee or cover sheet	
139	130	139	130 Non-English specification	
147	2,520	147	2,520 For filing a request for ex parte reexamination	
112	820*	112	920* Requesting publication of SIR prior to Examiner action	
113	1,840*	113	1,840* Requesting publication of SIR after Examiner action	
115	110	215	55 Extension for reply within first month	
116	400	216	200 Extension for reply within second month	
117	920	217	480 Extension for reply within third month	
118	1,440	218	720 Extension for reply within fourth month	
128	1,880	228	980 Extension for reply within fifth month	
119	320	219	160 Notice of Appeal	
120	320	220	160 Filing a brief in support of an appeal	
121	280	221	140 Request for oral hearing	
138	1,510	138	1,510 Petition to institute a public use proceeding	
140	110	240	55 Petition to revive - unavoidable	
141	1,280	241	640 Petition to revive - unintentional	
142	1,280	242	640 Utility issue fee (or reissue)	
143	460	243	230 Design issue fee	
144	620	244	310 Plant issue fee	
122	130	122	130 Petitions to the Commissioner	
123	50	123	50 Processing fee under 37 CFR 1.17(q)	
126	180	126	180 Submission of Information Disclosure Stmt	
581	40	581	40 Recording each patent assignment per property (times number of properties)	
148	740	246	370 Filing a submission after final rejection (37 CFR § 1.129(a))	
149	740	249	370 For each additional invention to be examined (37 CFR § 1.129(b))	
179	740	279	370 Request for Continued Examination (RCE)	
169	900	189	900 Request for expedited examination of a design application	
			Other fee (specify) _____	

*Reduced by Basic Filing Fee Paid SUBTOTAL (3) (\$ 0)

SUBMITTED BY		Complete (if applicable)		
Name (Print/Type)	Robert J. Wolff	Registration No. (Attorney/Agent)	34,948	Telephone 610-481-6150
Signature	Date February 25, 2002			

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TITLE OF THE INVENTION:

A PROCESS AND APPARATUS FOR THE PRODUCTION OF SYNTHESIS GAS

CROSS-REFERENCE TO RELATED APPLICATIONS

Not applicable.

STATEMENT REGARDING FEDERALLY SPONSORED RESEARCH OR
5 DEVELOPMENT

Not applicable.

BACKGROUND OF THE INVENTION

10 The present invention relates to a process and apparatus for the production of synthesis gas, particularly for but not necessarily limited to, use in the production of hydrocarbon liquid fuels (e.g. using the Fischer-Tropsch ("F-T") process), methanol (e.g. by catalytic hydrogenation of carbon monoxide), oxo-alcohols and dimethyl ether ("DME").

15 Natural gas may be found in remote locations both on- and offshore. It is generally expensive and impractical to transport natural gas from its source to a distant processing plant. One solution is to convert the gas on-site to a valuable and easily transportable product. In this way, the value of the natural gas may be increased.

20 Natural gas may be converted to synthesis gas (or "syngas") which is a mixture of carbon monoxide and hydrogen. Syngas may be converted to a solid or liquid synthetic fuel ("synfuel") or converted to methanol, oxo-alcohols or DME. For optimum conversion in the F-T process, the ratio of hydrogen to carbon monoxide is preferably about 2 to 1. The conversion products have less volume per unit mass (i.e. have a greater density) than the natural gas. Accordingly, it is more economical to transport conversion products 25 than a corresponding amount of natural gas.

Syngas may be produced using a heat exchange reforming ("HER") process. A conventional two-step HER process may use natural gas as feedstock and employs a

primary exothermic (or heat-generating) unit producing syngas, e.g. from natural gas and oxygen, coupled with a secondary endothermic (or heat-requiring) unit that uses at least a portion of the heat generated in the primary unit to produce further syngas, e.g. by a reforming reaction of natural gas and steam. In certain HERs, the syngas generated by the HER feeds the primary exothermic unit, while other HERs operate in parallel to the exothermic unit and augment the syngas production therein.

There are several methods of producing syngas from natural gas. Examples of these methods include:

- 10 (a) Steam-methane reforming ("SMR") which uses an endothermic catalysed reaction between natural gas and steam. There is a need to import carbon dioxide or otherwise remove excess hydrogen to achieve the required ratio of 2 to 1 for the relative proportions of hydrogen and carbon monoxide in the resultant syngas. In many applications (including F-T processes, methanol synthesis and other chemical processes), such an opportunity to import carbon dioxide and/or export any separated excess hydrogen may not be available and/or economical;
- 15 (b) Partial oxidation ("POX") of natural gas with pure oxygen which achieves a hydrogen to carbon monoxide ratio in the resultant syngas in the range from 1.6 - 1.8 to 1. Imported hydrogen is needed to achieve that required ratio of 2 to 1 for the relative proportions of hydrogen and carbon monoxide in the resultant syngas;
- 20 (c) Autothermal reforming ("ATR") which uses a partial oxidation burner followed by a catalyst bed with a feed of natural gas, steam and oxygen to produce the required 2 to 1 ratio for the relative proportions of hydrogen and carbon monoxide in the resultant syngas; and
- 25 (d) Catalytic partial oxidation ("CPO") which is the reaction of natural gas with oxygen over a catalyst that permits flameless partial combustion to hydrogen and carbon monoxide in the required relative proportions in the resultant syngas.

For POX, ATR and CPO, the oxidation reaction in the primary heat-generating unit is exothermic and, thus, the syngas is produced at elevated temperature. For

example, POX produces syngas at a temperature of from 1200 to 1400°C, ATR produces syngas at a temperature of from 900 to 1100°C and CPO produces syngas at a temperature of from 1000 to 1100°C.

- 5 The excess heat generated in these processes may be used to generate steam, for example in waste heat boilers, that can be used in steam turbines to generate power for air separation systems, air compressors and other equipment.

- 10 The excess heat may be used with additional natural gas and steam in a separate secondary unit to generate further syngas *via* steam-methane reforming. This process is the basis of the generic two-step HER process. In such a process, the high temperature syngas from the primary heat-generating unit is usually introduced to the shell-side of a shell and tube style steam-methane reformer. The tubes may contain conventional steam-methane reforming catalyst over which natural gas and steam react endothermically to form syngas. The heat from syngas on the shell-side of the reformer is used to drive the endothermic steam-methane reforming reaction. The syngas stream leaving the tubes can be separately collected and used to feed the primary exothermic syngas generator. Preferably, however, the syngas streams leaving the tubes are combined with the syngas on the shell-side to produce syngas having the desired ratio of hydrogen to carbon monoxide at a temperature of from 500 to 600°C.

- 15 A secondary unit in which reforming takes place over catalyst using heat taken from the primary heat-generating unit is known as a Heat Exchange Reformer. One such example is described in US-A-4919844 (Wang; published on 24th April 1990) and is called an Enhanced Heat Transfer Reformer (or "EHTR"). The disclosure of this patent is incorporated herein by reference. Other existing HER processes are disclosed in WO-A-98/32817 (Halmo *et al*; published on 30th July 1998), WO-A-00/09441 (Abbot; published on 24th February 2000), WO-A-00/03126 (Fjellhaug *et al*; published on 20th January 2000) and US-A-5362453 (Marsch; published on 8th November 1994). These disclosures are also incorporated herein by reference.

20 An example of an HER process is disclosed in USSN 09/965979 (filed on 27th September 2001 and claiming priority from GB0025150.4 filed on 13th October 2000) and this disclosure is incorporated herein by reference. In this example, a POX reactor

is used in combination with an EHTR. Hydrocarbon fuel gas is reacted with steam and/or oxygen gas in a syngas generation system to produce a syngas product stream. An oxidant gas is compressed to produce a compressed oxidant gas, at least a portion of which is combusted in the presence of combustion fuel gas to produce combustion
5 product gas. The combustion product gas is expanded to produce power and expanded combustion product gas. Heat from the expanded combustion product gas is recovered by using the expanded combustion product gas to heat steam by heat exchange to produce heated steam, at least a portion of which is used to provide at least a portion of any steam requirement for producing the syngas product stream in the syngas
10 generation system. Additionally or alternatively, at least a portion of the oxygen gas is provided using an ASU that is driven by at least a portion of the power generated by the expansion of the combustion product gas.

14
15 Syngas product feeding conversion processes will unavoidably contain carbon dioxide. For F-T synfuel processes that use cobalt catalysts, this carbon dioxide behaves like an inert. Whilst it can be vented downstream, the carbon and oxygen capture efficiency of the entire gas to liquid ("GTL") process is lower, which contributes to the greenhouse effect. It is thus desirable to recycle this carbon dioxide to the front-end
20 syngas generator. It is a primary objective of this invention to enable efficient recycle of carbon dioxide and affect its efficient conversion to useful carbon monoxide, while minimizing the amount of such recycle and usage of oxygen feedstock.

16
17 Loss of carbon dioxide and methane from natural gas conversion processes is undesirable for several reasons. First, these gases are well known to have "greenhouse
25 gas" properties. Secondly, valuable carbon atoms are being lost to the atmosphere thereby affecting the carbon efficiency and yield of the overall processes. Therefore, it is also an objective of the present invention to reduce the emission level of these
30 greenhouse gases and other pollutants, for example oxides of nitrogen ("NO_x"), and to recover at least some of the valuable carbon that is usually lost in natural gas conversion processes using HER technology for syngas generation.

In HER processes where hot gas is introduced to the shell-side of an HER, it is undesirable for the temperature of the syngas leaving the primary heat-generating unit to be too high as the mechanical integrity of the HER may be challenged. For example, the

metal of the HER may lose its physical strength and soften. Therefore, it is another objective of the present invention to reduce or eliminate the possibility of problems with the mechanical integrity of the HER resulting from excessive syngas temperature in natural gas conversion processes using HER technology.

5

The POX process can generate syngas with small amounts of solid carbon particles or soot. This soot could foul or erode the heat exchange surfaces in the downstream HER. It is thus another objective of this invention to reduce or eliminate the potential for problems arising for such solid carbon particles.

10

US-A-4731098 (Marsch; published on 15th March 1988) discloses a reformer in which natural gas and steam are reformed to produce syngas. The syngas is then mixed with natural gas and oxygen or air before the mixture leaves the reformer.

15

Water has been used as a diluent in the production of syngas. Examples of such use of water have been disclosed by P. Osterrieth and M. Quintana ("A New Approach to the Production of Custom-made Synthesis Gas Using Texaco's Partial Oxidation Technology"; Texaco Development Corporation; AIChE meeting Presentation, 6th March 1988) and by W. Francis Fong and M. E. Quintana ("HyTEX: A Novel Process for Hydrogen Production"; Texaco Development Corporation; NPRA 89th Annual Meeting, 17th-19th March 1991, San Antonio, Texas)

20

In meeting these objectives, it is also important that any modifications to existing HER processes do not affect adversely the yield of conversion products, the capital and/or operating costs and the level of power usage.

25

BRIEF SUMMARY OF THE INVENTION

It has been found that these objectives may be achieved with the introduction of a cooling stream of reactive diluent fluid to the syngas produced in the primary heat-generating unit to produce a cooled mixture of syngas and reactive diluent fluid and the subsequent reaction of at least two of the components of the mixture to either produce further carbon monoxide or to gasify solid carbon particles.

Hydrocarbon-containing fuel is exothermically reacted with an oxidant gas comprising molecular oxygen in a first reactor to produce an exothermically-generated syngas product. A stream of reactive diluent fluid is combined with a stream of said exothermically-generated syngas product to produce a reactive mixture and the reactive mixture is reacted in a second reactor to produce a reacted syngas product. If desired, this reacted syngas may be introduced into the secondary reforming unit in an HER process. One advantage of the invention is that the reacted syngas product is cooled before being introduced into the secondary unit thereby avoiding negatively affecting the mechanical integrity of the secondary unit.

10

If the reactive diluent fluid comprises gases produced downstream in the overall process that would otherwise be vented to the atmosphere or that would have to undergo treatment before venting to atmosphere, the level of pollutant emissions to the environment may be reduced and corresponding cost savings may be achievable from 15 the pollutant gas treatment processes.

15

Carbon dioxide and hydrogen present in the reactive mixture may be converted into water and valuable carbon monoxide. This conversion is particularly useful when the reactive diluent fluid is carbon dioxide. However, it still has useful application when 20 the reactive diluent fluid is not carbon dioxide but the source of hydrocarbon fuel (e.g. natural gas) contains significant quantities of carbon dioxide. The additional carbon monoxide produced may be used downstream to improve the yield of the natural gas conversion products. If the reactive diluent fluid comprises carbon dioxide that has been recycled from downstream processes then there is a further advantage in that the level 25 of carbon dioxide emission to the environment is reduced.

30

If the syngas is utilized in an F-T synfuel process, the gas exiting such a downstream process can contain significant amounts of carbon dioxide. Such gas typically also contains unconverted syngas as well as light hydrocarbons. It is particularly advantageous to this invention to recycle such carbon dioxide-comprising gas as the reactive diluent. Such gas can be recycled as diluent without further processing in which case the other components (other than carbon dioxide) would participate in the reaction, increasing the production of desired synfuel. Alternately, the carbon dioxide content of such gas can be isolated in an acid gas removal ("AGR") unit

for recycle to the front end of the process and the other components could be used as fuel. The carbon dioxide, steam, oxygenates and molecular hydrogen in the recycled diluent can participate in the gasification of soot.

- 5 A reverse water gas shift reaction may be used to convert the carbon dioxide and hydrogen into water and valuable carbon monoxide. Such a reaction is endothermic and, thus, uses heat from the reactive mixture thereby imposing additional cooling on the syngas and assisting in the overall ability to maintain mechanical integrity in the secondary reforming unit of the HER process.

10

In existing HER processes where carbon dioxide is recycled from downstream processes, the carbon dioxide is fed to the tube side of the HER unit of the synthesis gas generation system. In the tubes of the HER unit, the following two reactions take place:

15



- Reaction (I) is thermodynamically less favourable than reaction (II) and requires higher temperatures. The temperature at the exit of the HER tubes is necessarily lower than the temperature of the gas from the exothermic reactor. Therefore, the carbon dioxide is not completely converted when the syngas exits the tubes of the reformer unit. If the HER is a parallel type (such as an EHTR), this can lead to excessive costs associated with the recycle of carbon dioxide.

25

According to the present invention, carbon dioxide is converted to carbon monoxide in a reverse water gas shift reaction before being fed to the secondary reformer unit. The following reaction takes place in the reverse water gas shift reactor:

30



Reaction (III) is in equilibrium but the position of the equilibrium is pushed far over to the right hand side due to the high temperature of the syngas and the continual introduction of carbon dioxide. Therefore, by recycling carbon dioxide, injecting it into

the exothermically-generated syngas product produced in the primary heat-generating unit and subjecting the reactive mixture to a reverse water gas shift reaction, more carbon dioxide may be converted to useful carbon monoxide. This conversion minimizes the size of the carbon dioxide recycle loops and associated costs. In addition, the
5 reverse shift reaction zone assists in the gasification of any soot in the syngas from a POX-type exothermic unit, mitigating any erosion or fouling concerns in the surfaces of heat exchangers downstream, including HERs, boilers and preheaters. It can also eliminate the requirement of a scrubber that normally accompanies POX processes.

10 BRIEF DESCRIPTION OF SEVERAL VIEWS OF THE DRAWINGS

FIGURE 1 is a flowsheet describing one embodiment of the process of the present invention; and

FIGURE 2 is a flowsheet describing a hydrocarbon conversion process in which the process of Figure 1 is integrated with a downstream generic syngas conversion
15 process to produce hydrocarbon liquid fuels or other liquid products.

DETAILED DESCRIPTION OF THE INVENTION

According to one aspect of the present invention, there is provided a process for the production of syngas comprising carbon monoxide and molecular hydrogen, said
20 process comprising;

exothermically reacting hydrocarbon-containing fuel an oxidant gas comprising molecular oxygen in a first reactor to produce an exothermically-generated syngas product;

combining a stream of reactive diluent fluid with a stream of said exothermically-generated syngas product to produce a reactive mixture; and

reacting said mixture in a second reactor to produce a reacted syngas product.

The "reactive diluent fluid" includes any diluent fluid that is capable of cooling syngas by direct heat exchange and comprising at least one component that may react with at least
30 one component of the synthesis gas. The "reactive mixture" comprises cooled exothermically generated syngas product and reactive diluent fluid. The "reacted syngas product" includes the product syngas that has undergone a further reaction either to

produce further carbon monoxide or to remove solid carbon particles, e.g. soot, produced as a by-product of the oxidation reaction in the primary heat-generating unit.

The hydrocarbon fuel may be a solid or liquid fuel but it is preferably a gas. Natural gas
5 is the preferred fuel. Pure molecular oxygen is preferred as the oxidant gas over an oxidant gas comprising molecular oxygen such as air. Water may be present in the reaction to produce exothermically-generated syngas product (for example, if an ATR process is used). If water is present, it may be used in liquid form in which case it will vaporise immediately upon entry into the first reactor. However, the use of steam is
10 preferred.

An advantage of this invention is that the temperature of the exothermically-generated syngas product is reduced and may be controlled as required for downstream processing. The downstream mechanical integrity problems that may result from the high levels of heat generated in the primary heat-generating unit may be avoided and process operability may be improved by controlling the reduced temperature of the exothermically-generated syngas product.
15

Another advantage of this invention that any solid carbon present in the
20 exothermically-generated syngas product can be at least partially gasified mitigating fouling, erosion or plugging of downstream heat exchangers such as HERs, boilers or preheaters.

Where the reactive mixture comprises carbon dioxide, at least a portion of the
25 carbon dioxide may be reacted together with at least a portion of the molecular hydrogen in said mixture over a catalyst in a reverse water gas shift reaction zone to produce a carbon monoxide-enriched syngas product.

Where the reactive mixture comprises solid carbon particles, at least a portion of
30 the particles may be gasified by reaction with at least one other component of the mixture in a gasification zone to produce a solid carbon-depleted syngas product. The gasification reaction preferably occurs on the surface of a gasification reaction support structure and may be catalysed.

The process preferably further comprises endothermically reforming hydrocarbon-containing fuel gas with steam over a catalyst in a heat exchange reformer to produce a heat exchange-reformed syngas product. At least a portion of the heat required in the generation of said heat exchange-reformed syngas product is obtained by recovering heat from said reacted syngas product thereby cooling the reacted syngas product. Use of this heat in this way provides further overall cooling of the syngas. The heat exchange-reformed syngas product may be combined with the reacted syngas product prior to heat recovery.

- 5 When the reactive diluent fluid is a gas, the exothermically-generated syngas product is first cooled *via* sensible heat exchange. When the reactive diluent fluid is a liquid, initial cooling occurs *via* vaporisation and sensible heat exchange. The reactive diluent fluid may be recovered and recycled from downstream processing of syngas. The reactive diluent fluid may promote the gasification of any solid carbon particles or soot present in the reactive mixture. The reactive diluent fluid may be imported from an external source.

- 10 The reactive diluent fluid preferably comprises carbon dioxide. An advantage of using carbon dioxide as the diluent is that it may be readily converted to more useful carbon monoxide *via* a reverse water-gas shift reaction (see reaction (III)), resulting in more carbon monoxide being available for downstream processing. In addition, if the carbon dioxide has been recycled from downstream processes, the potential emission level of this greenhouse gas is reduced.

- 15 The reactive diluent fluid may comprise carbon dioxide separated, e.g. by acid gas recovery and recycled from downstream syngas or recovered and recycled from downstream processing of syngas. Alternately, the residual gas from a GTL reactor comprising carbon dioxide can be recycled without processing in an AGR unit. The reactive diluent may comprise the products of a combustion process which would contain a significant quantity of carbon dioxide. The combustion products may be selected from the group consisting of combustion furnace flue gases and gas turbine exhaust gas. The reactive diluent fluid may comprise carbon dioxide imported from an external source. For certain applications, the reactive diluent fluid may comprise carbon dioxide and methane either alone or together with other hydrocarbon(s) such as ethane, propane,

butane, pentane, hexane and/or their isomers. In a typical F-T based GTL process, the diluent may be a residual effluent of the reactor after separation of synfuel and water. In this case, it would comprise of carbon dioxide, unreacted carbon monoxide and molecular hydrogen, low molecular weight paraffins, olefins and oxygenates. The 5 recycling of these gases increases their utilization and increases the overall GTL process efficiency.

The reactive diluent fluid may comprise molecular hydrogen. The injection of hydrogen into the first syngas product pushes the position of the equilibrium in reaction 10 (III) in a reverse water gas shift reaction towards the carbon monoxide product side. This effect is advantageous because it promotes the conversion of carbon dioxide to carbon monoxide.

15 The use of carbon dioxide or molecular hydrogen as diluent is advantageous as both gases are capable of promoting the gasification of carbon components in the mixture of cooled exothermically-generated syngas product and reactive diluent fluid.

20 The reactive diluent fluid may comprise water. The water may be in the form of liquid water or steam or may comprise a combination of liquid water and steam. The injection of water is primarily to promote the gasification of carbon components in the mixture of cooled exothermically-generated syngas product and reactive diluent fluid.

25 The reacted syngas product from the reformer is preferably used in a downstream conversion process to produce conversion products selected from the group consisting of hydrocarbon liquid fuels, methanol, DME and oxo-alcohols.

In a second aspect of the present invention, there is provided a process for the production of syngas comprising carbon monoxide and molecular hydrogen, said process comprising;

30 exothermically reacting hydrocarbon-containing fuel with an oxidant gas comprising molecular oxygen in a first reactor to produce an exothermically-generated syngas product;

cooling an effluent stream of said exothermically-generated syngas product by combining reactive diluent fluid with said stream to produce a mixture comprising cooled

exothermically-generated syngas product and reactive diluent fluid, said mixture further comprising at least one component selected from the group consisting of carbon dioxide and solid carbon particles;

- 5 reacting together carbon dioxide in said mixture with molecular hydrogen in said mixture to produce a carbon monoxide-enriched syngas product; and/or
gasifying solid carbon particles in said mixture with at least one other component in said mixture to produce a solid carbon-depleted syngas product.

The step of the process to produce solid carbon-depleted syngas can be carried out
10 instead of the step to produce carbon monoxide-enriched syngas and vice versa.
Alternatively, the two steps can be carried out either sequentially or simultaneously.

In a third aspect of the present invention, there is provided a process for the production of syngas comprising carbon monoxide and molecular hydrogen, said process comprising:

- 15 exothermically reacting hydrocarbon-containing fuel gas with an oxidant gas comprising molecular oxygen in a first reactor to produce a first syngas product;
cooling an effluent stream of said first syngas product by combining reactive diluent fluid comprising carbon dioxide with said stream to produce a mixture of cooled first syngas product and reactive diluent fluid;
20 reacting at least a portion of the carbon dioxide in said mixture with at least a portion of the molecular hydrogen in said mixture over a catalyst in a reverse water gas shift reaction zone to produce a carbon monoxide-enriched syngas product;
endothermically reforming hydrocarbon-containing fuel gas with steam over a catalyst in a heat exchange reformer to produce a second syngas product; and
25 combining at least a portion of said second syngas product with at least a portion of the carbon monoxide-enriched syngas product to produce a combined syngas product,
wherein at least a portion of the heat generated in the exothermic reaction producing
30 said first syngas product is used to drive the endothermic reforming reaction.

In a fourth aspect of the present invention, there is provided apparatus for the production of syngas comprising carbon monoxide and molecular hydrogen, said apparatus comprising:

a first reactor in which hydrocarbon-containing fuel is reacted exothermically with an oxidant gas comprising molecular oxygen to produce an exothermically-generated syngas product;

5 conduit means for removing an effluent stream of said exothermically-generated syngas product from the first reactor;

means for combining a stream of reactive diluent fluid with said effluent stream to produce a reactive mixture; and

a second reactor in which said mixture reacts to produce a reacted syngas product.

10 The first reactor is preferably selected from the group consisting of a POX reactor, an ATR or a CPO reactor.

15 Where the reactive mixture comprises carbon dioxide, the second reactor preferably has a reverse water gas shift reaction zone in which at least a portion of the carbon dioxide and at least portion of the molecular hydrogen in the reactive mixture are reacted together over a catalyst to produce a carbon monoxide-enriched syngas.

20 Where the reactive mixture comprises solid carbon particles, the second reactor may have a gasification reaction zone in which at least a portion of the solid carbon particles is gasified by reaction with at least one other component of the reactive mixture to produce a solid carbon-depleted syngas.

25 The apparatus preferably further comprises a heat exchange reformer in which hydrocarbon-containing fuel gas is reformed endothermically with steam over a catalyst to produce a heat exchange-reformed syngas product, wherein at least a portion of the heat required in the generation of said heat exchange-reformed syngas product is obtained by recovering heat from said reacted syngas product thereby cooling the reacted syngas product.

30 The reformer is preferably a shell and tube style reformer in which the endothermic reforming reaction occurs within the tubes and the reacted syngas product is introduced to the shell-side. Most preferably, the reformer is an EHTR.

In a fifth aspect of the present invention, there is provided apparatus for the production of syngas comprising carbon monoxide and molecular hydrogen, said apparatus comprising:

- a first reactor in which hydrocarbon-containing fuel is reacted exothermically with an oxidant gas comprising molecular oxygen to produce an exothermically-generated syngas product;
 - 5 conduit means for removing an effluent stream of said exothermically generated syngas product from the first reactor;
 - means for combining reactive diluent gas comprising carbon dioxide with said effluent stream to produce a mixture comprising cooled first syngas product and reactive diluent gas, said mixture further comprising at least one component selected from the group consisting of carbon dioxide and solid carbon particles;
 - 10 a reverse water gas shift reaction zone in which carbon dioxide in said mixture is reacted together with molecular hydrogen in said mixture over a catalyst to produce a carbon monoxide-enriched syngas product; and/or
 - 15 a gasification reaction zone in which solid carbon particles in said mixture are gasified with at least one other component in said mixture to produce a solid carbon-depleted syngas product.
- 20 In a sixth aspect of the present invention, there is provided apparatus for the production of syngas comprising carbon monoxide and molecular hydrogen, said apparatus comprising:
- a first reactor in which hydrocarbon-containing fuel gas is reacted exothermically with an oxidant gas comprising molecular oxygen to produce a first syngas product;
 - 25 conduit means for removing an effluent stream of said first syngas product from the first reactor;
 - means for combining reactive diluent gas comprising carbon dioxide with said effluent stream to produce a mixture of cooled first syngas product and reactive diluent gas;
 - a reverse water gas shift reaction zone in which at least a portion of the carbon dioxide in
 - 30 said mixture is reacted with at least a portion of the molecular hydrogen in said mixture over a catalyst to produce a carbon monoxide-enriched syngas product; and
 - a heat exchange reformer in which hydrocarbon-containing fuel gas is reformed endothermically with steam over a catalyst to produce a second syngas product and in which at least a portion of said second syngas product is combined with at least a portion

of said carbon monoxide-enriched syngas product to produce a combined syngas product, wherein at least a portion of the heat generated in the exothermic reaction producing said first syngas product is used to drive the endothermic reforming reaction.

- 5 The first reactor is preferably a POX reactor as this reactor produces the highest temperature syngas (when compared with ATR and CPO) and the higher the temperature of the syngas from the primary heat-generating unit, the higher the conversion of carbon dioxide in the reactive diluent and the better the efficiency of downstream HER processing. The POX reactor is preferably used in combination with
- 10 an EHTR as the heat exchange reformer.

EXAMPLE

Referring to Figure 1, a stream 2 of natural gas is preheated by indirect heat exchange 8, hydrodesulfurized as required, and divided into a first portion 4 and a second portion 6. The first portion 4 is introduced into a POX reactor 12. A stream 14 of oxygen is pre-heated by indirect heat exchange 16 and the pre-heated oxygen stream 18 is also fed to the POX reactor 12. The natural gas and the oxygen are reacted together in the POX reactor 12 to produce first syngas product. A stream 20 of first syngas product is removed from the POX reactor 12 at a temperature of from 1200 to 1400°C.

A stream 22 comprising carbon dioxide is introduced to and cools the first syngas product stream 20. The cooled stream 24 is fed to a reverse water gas shift reactor 26 in which at least a portion of the carbon dioxide from the cooled stream 24 is reacted with at least a portion of the hydrogen from the cooled stream 24 to produce carbon monoxide and water. The catalytic reaction is endothermic and, thus, a further cooling effect on the syngas is observed. A stream 28 of carbon monoxide-enriched syngas is removed from the reverse water gas shift reactor 26 and introduced to the shell-side of an EHTR 30.

A stream 32 of steam is introduced to the second portion 6 of the natural gas and the combined stream 34 is pre-heated by indirect heat exchange 36. The pre-heated combined stream 38 is introduced to the tube-side of the EHTR 30. The tubes of the EHTR 30 contain conventional steam-methane reforming catalyst and the natural gas

and the steam react to form second syngas product. Heat from the shell-side of the EHTR 30 provided at least in part by the carbon monoxide-enriched syngas, is used to drive the endothermic catalytic steam-methane reforming reaction.

- 5 The second syngas product leaving the tubes of the EHTR 30 is combined with the first syngas product to form a combined syngas product. A stream 40 of combined syngas product is removed for downstream processing, in particular for the synthesis of hydrocarbon liquid fuels (e.g. by the F-T process), methanol (e.g. by the catalytic hydrogenation of carbon monoxide), exo-alcohols and DME.

10

Table 1 contains data for the composition of various streams in the process of Figure 1 calculated in a computer simulation.

STREAM ID	2	4	6	18	20	22	24	28	38	40
STREAM	NG FEED	NG TO POX	NG TO EHTR	POX O2	POX OUT	FT OFFGAS	QUENCH ED	CATBED UT	EHTR FEED	EHTR OUT
Temperature F	60	685	685	449.3	2450	100	2269.7	2185.7	950	1094.2
Pressure psia	515	494	494	460	412	600	412	412	484	412
Mole Flow lbmol/hr	18542	14471	46553	9187	43416	2301	45717	45908	14499	68238
Enthalpy MMBtu/hr	-625.0	-371.6	-119.5	24.3	-348.3	-390.9	-739.2	-739.2	-1055.0	-1814.0
COMPONENTS										
Mole Flow lbmol/hr										
H2	440.4	141.6	25213.8				23774.9	141.6	36219.7	
C1	17564.4	13290.9	4273.5	200.1			200.1	104.3	4273.5	877.1
C2	585.9	443.4	142.6						142.6	
C3	100.1	75.8	24.4						24.4	
C4	33.4	25.3	8.1						8.1	
C5	11.1	8.4	2.7						2.7	
C6	7.4	5.6	1.8						1.8	
CD	131.6	99.6	32.0						32.0	
CM										
WA										
O2										
AR										
N2										
Mole percent										
H2	107.5	81.4	26.2						45.9	45.9
C1	94.70%	91.80%	3.00%	58.10%	0.50%		55.20%	51.80%	1.00%	53.10%
C2+	PRESENT	PRESENT	PRESENT	0.40%	0.70%		0.40%	0.20%	29.50%	1.30%
CD	0.70%	0.70%	0.70%	1.70%	1.70%		1.70%	6.70%	2.90%	PRESENT
CM								30.10%	33.90%	
WA								7.80%	7.40%	
O2									10.90%	
AR									67.90%	
N2	0.60%	0.60%	0.60%	99.50%	0.50%		0.10%	0.10%	0.20%	14.90%
				0.60%	0.60%		0.20%	0.20%	0.20%	0.20%

Referring now to Figure 2, a syngas generation system 42 of the type depicted in Figure 1 is fed by a stream 2 of hydrocarbon fuel gas, a stream 14 of oxygen or air and a stream 32 of steam. A stream 40 of syngas is removed from the syngas generation system 42 and fed to a syngas conversion system 44. The syngas conversion system

- 5 44 may use an F-T process to synthesize liquid hydrocarbons or involve the synthesis of methanol, DME or oxo-alcohols. A stream 46 of raw conversion product is removed from the syngas conversion system 44 and upgraded and refined 50 to produce the liquid products 52.

- 10 A stream 22 of reactive diluent gas is recycled from the syngas conversion system 44 to the syngas generation system 42. A recycle stream 54 may also be taken from the product upgrading and refining process 50.

- 15 It will be appreciated that the invention is not restricted to the details described above with reference to the preferred embodiments but that numerous modifications and variations can be made without departing from the spirit or scope of the invention as defined in the following claims.

20

CLAIMS

1. A process for the production of synthesis gas ("syngas") comprising carbon monoxide and molecular hydrogen, said process comprising:
 - 5 exothermically reacting hydrocarbon-containing fuel with an oxidant gas comprising molecular oxygen in a first reactor to produce an exothermically-generated syngas product;
 - 10 combining a stream of reactive diluent fluid with a stream of said exothermically-generated syngas product to produce a reactive mixture; and reacting said mixture in a second reactor to produce a reacted syngas product.
- 15 2. The process according to Claim 1, wherein the oxidant gas consists of molecular oxygen.
- 20 3. The process according to Claim 1, wherein the hydrocarbon fuel is reacted with the oxidant gas in the presence of water.
- 25 4. The process according to Claim 1 wherein the reactive mixture comprises carbon dioxide, at least a portion of which is reacted together with at least a portion of the molecular hydrogen in said mixture over a catalyst in a reverse water gas shift reaction zone to produce a carbon monoxide-enriched syngas product.
- 30 5. The process according to Claim 1 wherein the reactive mixture comprises solid carbon particles, at least a portion of which is gasified by reaction with at least one other component of the mixture in a gasification zone to produce a solid carbon-depleted syngas product.
6. The process according to Claim 1 further comprising endothermically reforming hydrocarbon-containing fuel gas with steam over a catalyst in a heat exchange reformer to produce a heat exchange-reformed syngas product, wherein at least a portion of the heat required in the generation of said heat exchange-reformed syngas product is obtained by recovering heat from said reacted syngas product thereby cooling the reacted syngas product.

7. The process according to claim 6 wherein said heat exchange-reformed syngas product is combined with said reacted syngas product prior to heat recovery.

5 8. The process according to Claim 1 wherein the reactive diluent fluid is a gas thereby cooling the exothermically-generated syngas product via sensible heat exchange.

9. The process according to Claim 1 wherein the reactive diluent fluid is a liquid
10 thereby cooling the exothermically-generated syngas product via vaporisation and sensible heat exchange.

10. The process according to Claim 1 wherein the reactive diluent fluid is recovered and recycled from downstream processing of syngas.

15 11. The process according to Claim 1 wherein the reactive diluent fluid comprises carbon dioxide.

20 12. The process according to Claim 11 wherein the reactive diluent fluid comprises carbon dioxide separated and recycled from downstream syngas.

13. The process according to Claim 11 wherein the reactive diluent fluid comprises the products of a combustion process.

25 14. The process according to Claim 13 wherein the combustion products are selected from the group consisting of combustion furnace flue gases and gas turbine exhaust gas.

15. The process according to Claim 11 wherein the reactive diluent fluid comprises carbon dioxide imported from an external source.

30 16. The process according to Claim 11 wherein the reactive diluent fluid further comprises a component selected from the group consisting of methane and other hydrocarbon(s).

17. The process according to Claim 1 wherein the reactive diluent fluid comprises molecular hydrogen.
18. The process according to Claim 1 wherein the reactive diluent fluid comprises
5 water.
19. The process according to Claim 18 wherein the water is in the form of liquid water.
- 10 20. The process according to Claim 18 wherein at least a portion of the water is in the form of steam.
- 15 21. The process according to Claim 1 wherein the reacted syngas product is used in a downstream conversion process to produce conversion products selected from the group consisting of hydrocarbon liquid fuels, methanol, DME and oxo-alcohols.
- 20 22. A process for the production of syngas comprising carbon monoxide and molecular hydrogen, said process comprising;
comprising exothermically reacting hydrocarbon-containing fuel with an oxidant gas comprising molecular oxygen in a first reactor to produce an exothermically-generated syngas product;
- 25 cooling an effluent stream of said exothermically-generated syngas product by combining reactive diluent fluid with said stream to produce a mixture comprising cooled exothermically-generated syngas product and reactive diluent fluid, said mixture further comprising at least one component selected from the group consisting of carbon dioxide and solid carbon particles;
- reacting together carbon dioxide in said mixture with molecular hydrogen in said mixture to produce a carbon monoxide-enriched syngas product; and/or
30 gasifying solid carbon particles in said mixture with at least one other component in said mixture to produce a solid carbon-depleted syngas product.
23. A process for the production of syngas comprising carbon monoxide and molecular hydrogen, said process comprising:

exothermically reacting hydrocarbon-containing fuel gas with an oxidant gas comprising molecular oxygen in a first reactor to produce a first syngas product;

5 cooling an effluent stream of said first syngas product by combining reactive diluent fluid comprising carbon dioxide with said stream to produce a mixture of cooled first syngas product and reactive diluent fluid;

10 reacting at least a portion of the carbon dioxide in said mixture with at least a portion of the molecular hydrogen in said mixture over a catalyst in a reverse water gas shift reaction zone to produce a carbon monoxide-enriched syngas product;

15 endothermically reforming hydrocarbon-containing fuel gas with steam over a catalyst in a heat exchange reformer to produce a second syngas product; and

20 combining at least a portion of said second syngas product with at least a portion of the carbon monoxide-enriched syngas product to produce a combined syngas product,

25 wherein at least a portion of the heat generated in the exothermic reaction producing said first syngas product is used to drive the endothermic reforming reaction.

24. Apparatus for the production of syngas comprising carbon monoxide and molecular hydrogen, said apparatus comprising:

30 a first reactor in which hydrocarbon-containing fuel is reacted exothermically with an oxidant gas comprising molecular oxygen to produce an exothermically-generated syngas product;

25 conduit means for removing an effluent stream of said exothermically-generated syngas product from the first reactor;

 means for combining a stream of reactive diluent fluid with said effluent stream to produce a reactive mixture; and

30 a second reactor in which said mixture reacts to produce a reacted syngas product.

25. Apparatus according to Claim 24 wherein the first reactor is selected from the group consisting of a partial oxidation ("POX") reactor, an autothermal reformer ("ATR") and a catalytic partial oxidation ("CPO") reactor.

26. Apparatus according to Claim 24 wherein the reactive mixture comprises carbon dioxide and the second reactor has a reverse water gas shift reaction zone in which at least a portion of the carbon dioxide and at least portion of the molecular hydrogen in said mixture are reacted together over a catalyst to produce a carbon monoxide-enriched
5 syngas product.

27. Apparatus according to Claim 24 wherein the reactive mixture comprises solid carbon particles and the second reactor has a gasification reaction zone in which at least a portion of the solid carbon particles is gasified by reaction with at least one other
10 component of the mixture to produce a solid carbon-depleted syngas product.

28. Apparatus according to Claim 24 further comprising a heat exchange reformer in which hydrocarbon-containing fuel gas is reformed endothermically with steam over a catalyst to produce a heat exchange-reformed syngas product, wherein at least a portion
15 of the heat required in the generation of said heat exchange-reformed syngas product is obtained by recovering heat from said reacted syngas product thereby cooling the reacted syngas product.

29. Apparatus according to Claim 28 wherein the heat exchange reformer is a shell
20 and tube style reformer in which the endothermic reforming reaction occurs within the tubes and the reacted syngas product is introduced to the shell-side.

30. Apparatus according to Claim 28 wherein the reformer is an enhanced heat transfer reformer ("EHTR").
25

31. Apparatus for the production of syngas comprising carbon monoxide and molecular hydrogen, said apparatus comprising:
30 a first reactor in which hydrocarbon-containing fuel is reacted exothermically with an oxidant gas comprising molecular oxygen to produce an exothermically-generated syngas product;
 conduit means for removing an effluent stream of said exothermically generated syngas product from the first reactor;
 means for combining reactive diluent gas comprising carbon dioxide with said effluent stream to produce a mixture comprising cooled first syngas product

and reactive diluent gas, said mixture further comprising at least one component selected from the group consisting of carbon dioxide and solid carbon particles;

5 a reverse water gas shift reaction zone in which carbon dioxide in said mixture is reacted together with molecular hydrogen in said mixture over a catalyst to produce a carbon monoxide-enriched syngas product; and/or

10 a gasification reaction zone in which solid carbon particles in said mixture are gasified with at least one other component in said mixture to produce a solid carbon-depleted syngas product.

10 32. Apparatus for the production of syngas comprising carbon monoxide and molecular hydrogen, said apparatus comprising:

15 a first reactor in which hydrocarbon-containing fuel gas is reacted exothermically with an oxidant gas comprising molecular oxygen to produce a first syngas product;

20 conduit means for removing an effluent stream of said first syngas product from the first reactor;

25 means for combining reactive diluent gas comprising carbon dioxide with said effluent stream to produce a mixture of cooled first syngas product and reactive diluent gas;

30 a reverse water gas shift reaction zone in which at least a portion of the carbon dioxide in said mixture is reacted with at least a portion of the molecular hydrogen in said mixture over a catalyst to produce a carbon monoxide-enriched syngas product; and

35 a heat exchange reformer in which hydrocarbon-containing fuel gas is reformed endothermically with steam over a catalyst to produce a second syngas product and in which at least a portion of said second syngas product is combined with at least a portion of said carbon monoxide-enriched syngas product to produce a combined syngas product, wherein at least a portion of the heat generated in the exothermic reaction producing said first syngas product is used to drive the endothermic reforming reaction.

33. Apparatus according to Claim 32 wherein the first reactor is a partial oxidation ("POX") reactor and the reformer is an EHTR.

ABSTRACT OF THE DISCLOSURE

- 5 Reactive diluent fluid is introduced into a stream of synthesis gas (or "syngas") produced in a heat-generating unit such as a partial oxidation ("POX") reactor to cool the syngas and form a mixture of cooled syngas and reactive diluent fluid. Carbon dioxide and/or carbon components and/or hydrogen in the mixture of cooled syngas and reactive diluent fluid is reacted with at least a portion of the reactive diluent fluid in the mixture to
- 10 produce carbon monoxide-enriched syngas which may be fed into a secondary reformer unit such as an enhanced heat transfer reformer in a heat exchange reformer process. An advantage of the invention is that problems with the mechanical integrity of the secondary unit arising from the high temperature of the syngas from the heat-generating unit are avoided.
- 15

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**DECLARATION FOR UTILITY OR
DESIGN
PATENT APPLICATION
(37 CFR 1.63)**

Declaration Submitted with Initial Filing

OR

Declaration Submitted after Initial Filing (surcharge (37 CFR 1.16 (e)) required)

Attorney Docket Number	06244 USA
First Named Inventor	Shou-I Wang
COMPLETE IF KNOWN	
Application Number	/
Filing Date	
Group Art Unit	
Examiner Name	

As a below named inventor, I hereby declare that:

My residence, mailing address, and citizenship are as stated below next to my name.

I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled:

A Process and Apparatus For The Production of Synthesis Gas

(Title of the Invention)

the specification of which

 is attached hereto

OR

 was filed on (MM/DD/YYYY) as United States Application Number or PCT InternationalApplication Number and was amended on (MM/DD/YYYY) (if applicable)

I hereby state that I have reviewed and understand the contents of the above identified specification, including the claims, as amended by any amendment specifically referred to above.

I acknowledge the duty to disclose information which is material to patentability as defined in 37 CFR 1.56, including for continuation-in-part applications, material information which became available between the filing date of the prior application and the national or PCT international filing date of the continuation-in-part application.

I hereby claim foreign priority benefits under 35 U.S.C. 119(a)-(d) or (f), or 365(b) of any foreign application(s) for patent, inventor's or plant breeder's rights certificate(s), or 365(a) of any PCT international application which designated at least one country other than the United States of America, listed below and have also identified below, by checking the box, any foreign application for patent, inventor's or plant breeder's rights certificate(s), or any PCT international application having a filing date before that of the application on which priority is claimed.

Prior Foreign Application Number(s)	Country	Foreign Filing Date (MM/DD/YYYY)	Priority Not Claimed	Certified Copy Attached? YES	Certified Copy Attached? NO
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 Additional foreign application numbers are listed on a supplemental priority data sheet PTO/SB/02B attached hereto.

[Page 1 of 2]

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I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under 18 U.S.C. 1001 and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

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Additional inventors are being named on the 1 supplemental Additional Inventor(s) sheet(s) PTO/SB/02A attached hereto.

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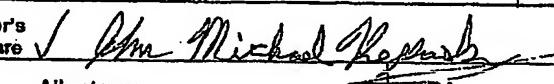
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DECLARATION

ADDITIONAL INVENTOR(S) Supplemental Sheet Page 1 of 1

Name of Additional Joint Inventor, if any:		<input type="checkbox"/> A petition has been filed for this unsigned inventor	
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Given Name (first and middle [if any])		Family Name or Surname	
Inventor's Signature			Date
Residence: City	State	Country	Citizenship
Mailing Address			
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Name of Additional Joint Inventor, if any:		<input type="checkbox"/> A petition has been filed for this unsigned inventor	
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Inventor's Signature			Date
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STATEMENT UNDER 37 CFR 3.73(b)Applicant/Patent Owner: Shou-I Wang

Application No./Patent No.: _____ Filed/Issue Date: _____

Entitled: **A Process and Apparatus For The Production of Synthesis Gas**

Air Products and Chemicals, Inc. _____, a _____ corporation

(Name of Assignee) (Type of Assignee, e.g., corporation, partnership, university, government agency, etc.)

states that it is:

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[NOTE: A separate copy (i.e., the original assignment document or a true copy of the original document) must be submitted to Assignment Division in accordance with 37 CFR Part 3, if the assignment is to be recorded in the records of the USPTO. See MPEP 302.08]

The undersigned (whose title is supplied below) is authorized to act on behalf of the assignee.

25 February 2002
DateWilliam F. MarshTyped or printed nameW/F/MSignatureAssistant General Counsel, PatentsTitle

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Application Number	
Filing Date	
First Named Inventor	Shou-I Wang
Title	A Process and Apparatus For The...
Group Art Unit	
Examiner Name	
Attorney Docket Number	06244 USA

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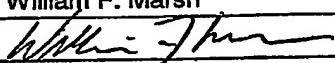
Fax

I am the:

Applicant/Inventor.

Assignee of record of the entire interest. See 37 CFR 3.71.
Statement under 37 CFR 3.73(b) is enclosed. (Form PTO/SB/96).

SIGNATURE of Applicant or Assignee of Record

Name	William F. Marsh
Signature	
Date	25 February 2002

NOTE: Signatures of all the inventors or assignees of record of the entire interest or their representative(s) are required. Submit multiple forms if more than one signature is required, see below*.

*Total of 1 forms are submitted.

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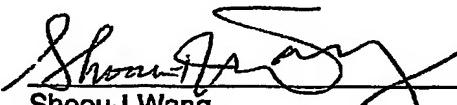
For value received, we, Shoou-I Wang, Shankar Nataraj, and John Michael Repasky, hereby sell, assign, and transfer to **AIR PRODUCTS AND CHEMICALS, INC.**, a corporation of the State of Delaware, having an office at 7201 Hamilton Boulevard, Allentown, PA 18195-1501, the entire right, title, and interest in and to the invention relating to

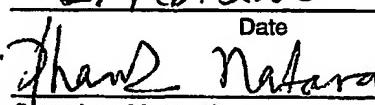
A Process and Apparatus For The Production of Synthesis Gas

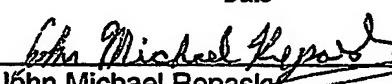
described in our application for Letters Patent of the United States (identified by Docket No. 06244 USA) executed of even date herewith, in and to all Letters Patent which may be issued upon said application, in and to any divisional or reissue applications based thereon, and in and to all Letters Patent upon said invention or improvements which may be granted in foreign countries. We hereby also assign and convey to said **AIR PRODUCTS AND CHEMICALS, INC.**, all the rights accruing to us by virtue of the International Convention for the Protection of Industrial Property (Art. 4), including the right to apply for and to have patents issued in its own name.

And we hereby authorize and request the Commissioner of Patents and Trademarks of the United States and the Officials of the Patent Offices of all other countries to issue the Letters Patent of their respective countries to said **AIR PRODUCTS AND CHEMICALS, INC.**, as assignee of the entire right, title, and interest in and to the same.

And we hereby promise and agree to execute all papers and perform all acts necessary to secure to and vest in said **AIR PRODUCTS AND CHEMICALS, INC.**, its successors and assigns, the rights conveyed as herein set forth.


Shoou-I Wang (L.S.)

21 Feb. 2002
Date

Shankar Nataraj (L.S.)

21 Feb. 2002
Date

John Michael Repasky (L.S.)

21 Feb. 2002
Date

1/2

2022-07-22 = 2022-07-22

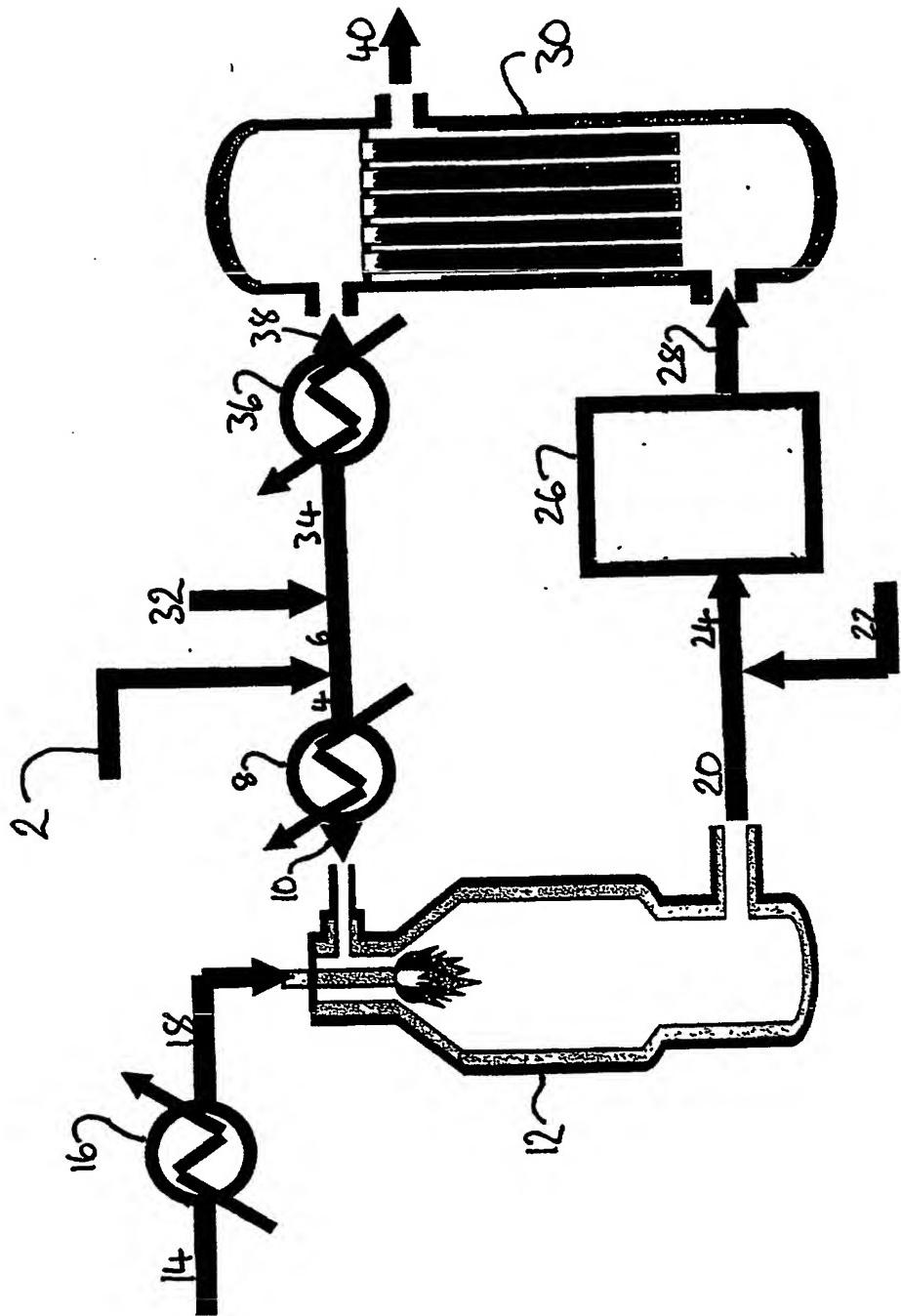


FIGURE 1

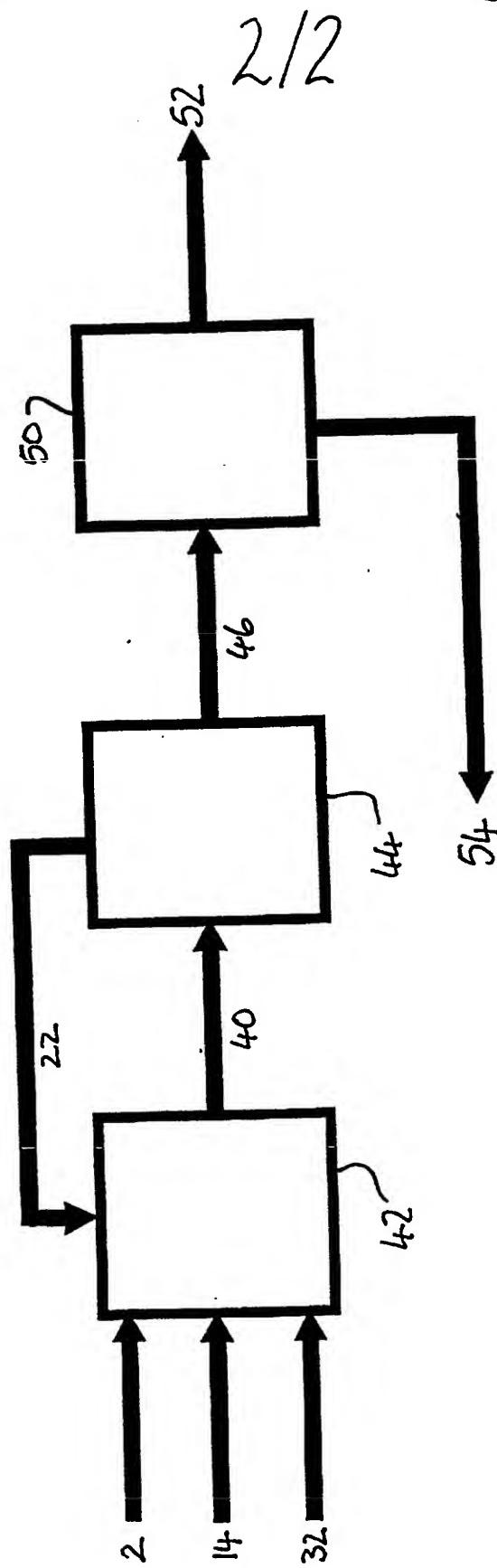


FIGURE 2

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